

1.5

$$q'' = -k \frac{T_2 - T_1}{L}$$

$$= -1.4 \frac{\text{W}}{\text{mK}} \frac{10^\circ\text{C} - 17^\circ\text{C}}{0.2 \text{ m}}$$

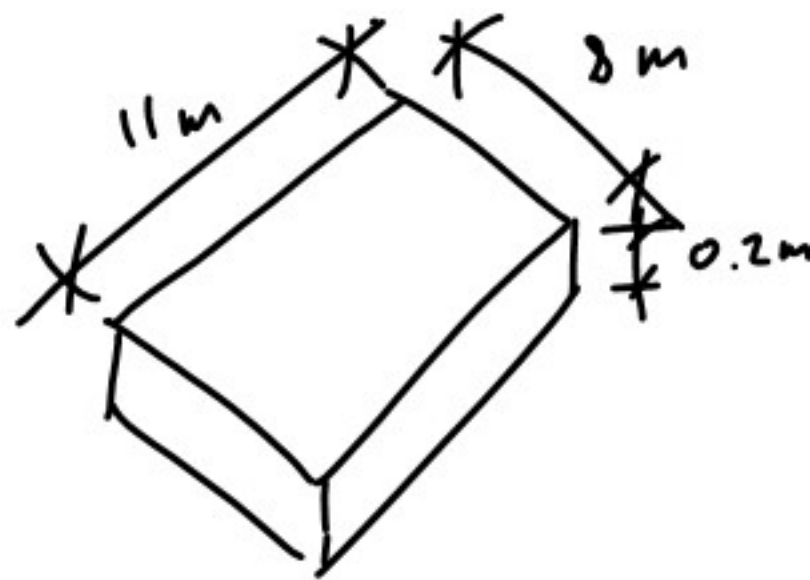
$$= -1.4 \frac{\text{W}}{\text{mK}} \frac{-7^\circ\text{C}}{0.2 \text{ m}}$$

$$= -1.4 \frac{\text{W}}{\text{mK}} \frac{-7 \text{ K}}{0.2 \text{ m}}$$

$$= 49 \frac{\text{W}}{\text{m}^2}$$

$$q = 49 \frac{\text{W}}{\text{m}^2} \cdot 11 \text{ m} \cdot 8 \text{ m} = \boxed{4312 \text{ W}}$$

The concrete slab of a basement is 11 m long, 8 m wide, and 0.20 m thick. During the winter, temperatures are nominally  $17^\circ\text{C}$  and  $10^\circ\text{C}$  at the top and bottom surfaces, respectively. If the concrete has a thermal conductivity of  $1.4 \text{ W/m}\cdot\text{K}$ , what is the rate of heat loss through the slab? If the basement is heated by a gas furnace operating at an efficiency of  $\eta_f = 0.90$  and natural gas is priced at  $C_g = \$0.02/\text{MJ}$ , what is the daily cost of the heat loss?



$$A = 11 \text{ m} \cdot 8 \text{ m}$$

$$W_f \eta_f = 2$$

$$W_f = \frac{2}{\eta_f} = \frac{9312}{0.9} = 4791 \text{ W}$$

$$\begin{aligned} W_f \text{ 1 day} &= 4791 \text{ W 1 day} \frac{24 \text{ h}}{1 \text{ day}} \frac{60 \text{ min}}{1 \text{ h}} \frac{60 \text{ s}}{1 \text{ min}} = 4.19 \times 10^8 \text{ Ws} \\ &= 4.19 \times 10^8 \text{ J} \\ &= 419 \text{ MJ} \end{aligned}$$

$$419 \text{ MJ} \frac{0.02}{\text{MJ}} = \boxed{58.28}$$

1.6

The heat flux through a wood slab 50 mm thick, whose inner and outer surface temperatures are 40 and 20°C, respectively, has been determined to be 40 W/m<sup>2</sup>. What is the thermal conductivity of the wood?

$$q'' = -k \frac{T_2 - T_1}{L}$$

$$40 \frac{\text{W}}{\text{m}^2} = -k \frac{20^\circ\text{C} - 40^\circ\text{C}}{50 \text{ mm}}$$

$$- \frac{40 \frac{\text{W}}{\text{m}^2} \cdot 50 \text{ mm}}{20^\circ\text{C} - 40^\circ\text{C}} = k = 100 \frac{\text{W} \cdot \text{mm}}{\text{m}^2 \cdot ^\circ\text{C}} \cdot \frac{1 \text{ m}}{1000 \text{ mm}} = 0.1 \frac{\text{W}}{\text{m} \cdot ^\circ\text{C}} = \boxed{0.1 \frac{\text{W}}{\text{m} \cdot \text{K}}}$$

1.10

A wall is made from an inhomogeneous (nonuniform) material for which the thermal conductivity varies through the thickness according to  $k = ax + b$ , where  $a$  and  $b$  are constants. The heat flux is known to be constant. Determine expressions for the temperature gradient and the temperature distribution when the surface at  $x = 0$  is at temperature  $T_1$ .

$$q'' = -k \frac{dT}{dx}$$

$$q'' = -(ax + b) \frac{dT}{dx}$$

$$\int \frac{-q''}{ax + b} dx = \int dT$$

$$-q'' \frac{\log(ax + b)}{a} + C = T$$

$$q'' = h(T_s - T_\infty)$$

You've experienced convection cooling if you've ever extended your hand out the window of a moving vehicle or into a flowing water stream. With the surface of your hand at a temperature of  $30^\circ\text{C}$ , determine the convection heat flux for (a) a vehicle speed of 40 km/h in air at  $-8^\circ\text{C}$  with a convection coefficient of  $40 \text{ W/m}^2 \cdot \text{K}$  and (b) a velocity of 0.2 m/s in a water stream at  $10^\circ\text{C}$  with a convection coefficient of  $900 \text{ W/m}^2 \cdot \text{K}$ . Which condition would *feel* colder? Contrast these results with a heat flux of approximately  $30 \text{ W/m}^2$  under normal room conditions.

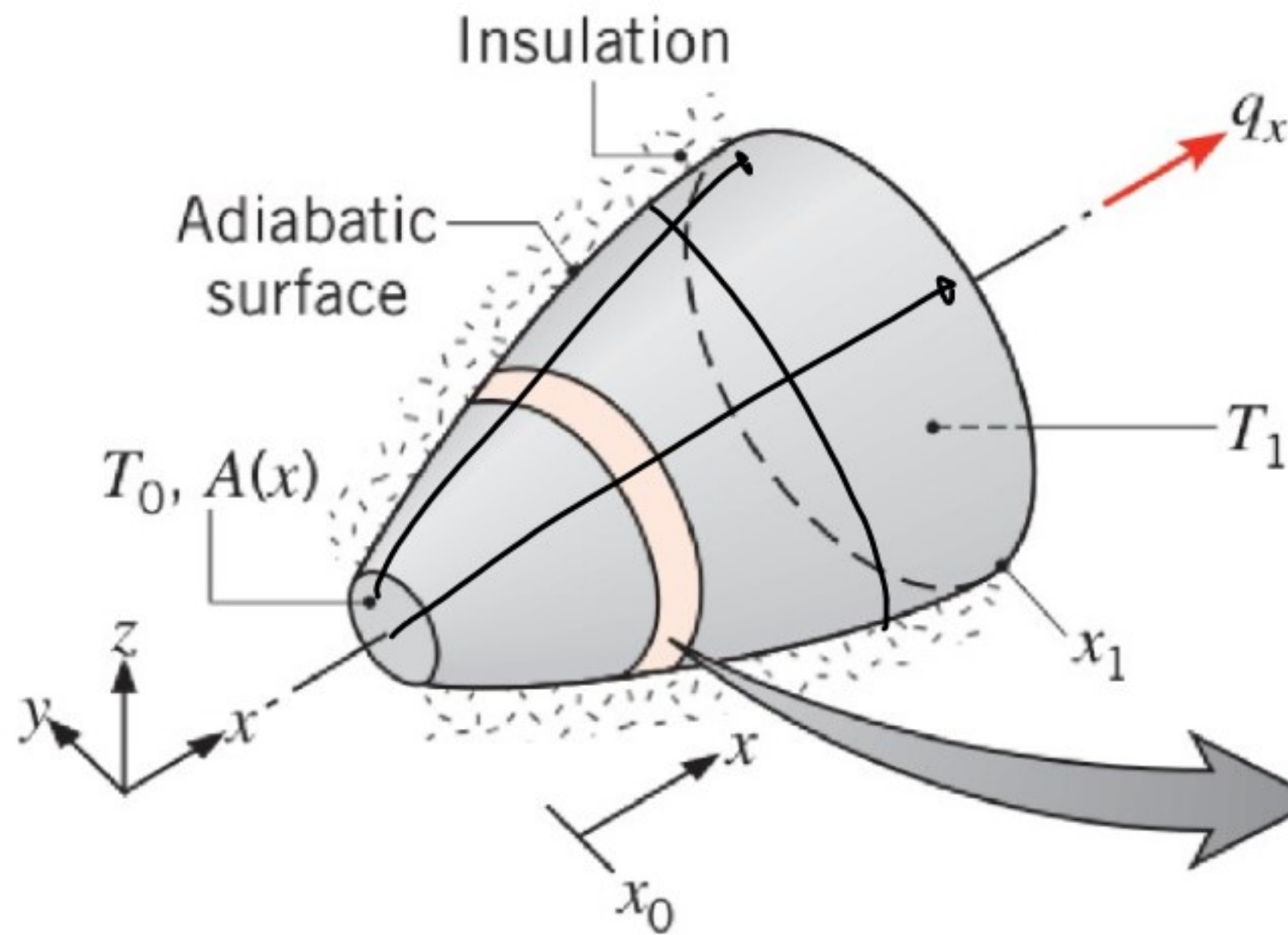
$$\text{a. } q'' = 40 \frac{\text{W}}{\text{m}^2 \cdot \text{K}} (30^\circ\text{C} - (-8^\circ\text{C}))$$

$$= 1520 \frac{\text{W}}{\text{m}^2}$$

$$\text{b. } q'' = 900 \frac{\text{W}}{\text{m}^2 \cdot \text{K}} (30^\circ\text{C} - 10^\circ\text{C})$$

$$= 18000 \frac{\text{W}}{\text{m}^2}$$

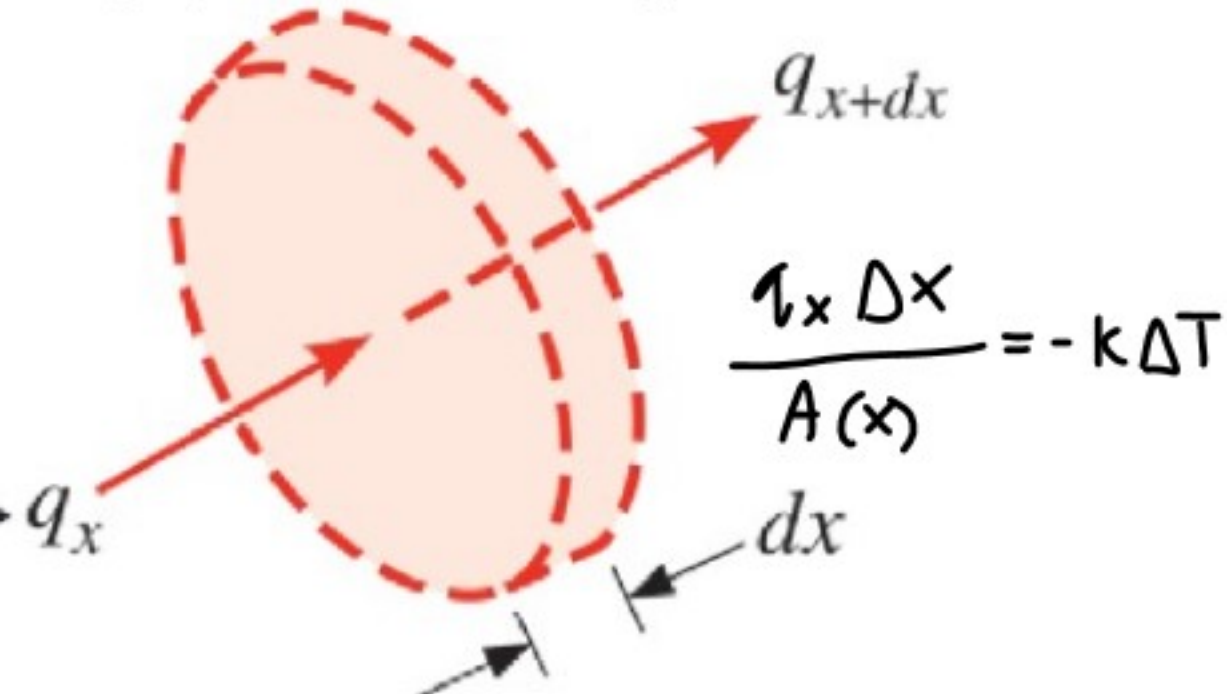
# 1.5 D Conduction



$$q_x = -k A(x) \frac{\partial T}{\partial x}$$

$$\frac{q_x}{A(x)} \partial x = -k \partial T$$

$$q_x \int \frac{1}{A(x)} dx = -k \int dT$$



$$q_x \int \frac{1}{A(x)} dx = -k \int_{T_1}^T dT$$

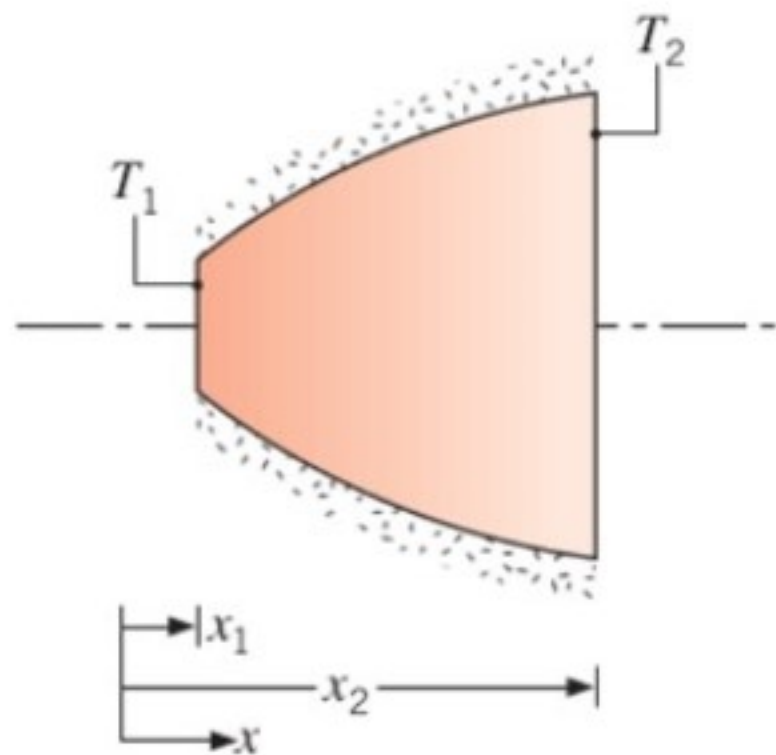
$$q_x \int_{x_1}^x \frac{\pi}{\pi a^2 x} dx = -k(T - T_1)$$

$$\frac{\pi q_x}{\pi a^2} \ln(x) \Big|_{x_1}^x = -k(T - T_1)$$

$$\frac{\pi q_x}{\pi a^2} (\ln(x) - \ln(x_1)) = -k(T - T_1)$$

The diagram shows a conical section fabricated from pure aluminum. It is of circular cross section having diameter  $D = ax^{1/2}$ , where  $a = 0.5 \text{ m}^{1/2}$ . The small end is located at  $x_1 = 25 \text{ mm}$  and the large end at  $x_2 = 125 \text{ mm}$ . The end temperatures are  $T_1 = 600 \text{ K}$  and  $T_2 = 400 \text{ K}$ , while the lateral surface is well insulated.

$$\begin{aligned} A(x) &= \pi r^2 = \pi \frac{D^2}{4} \\ &= \pi \frac{(ax^{1/2})^2}{4} \\ &= \frac{\pi}{4} a^2 x \end{aligned}$$



$$\frac{\pi q_x}{\pi a^2} \ln\left(\frac{x}{x_1}\right) = -k(T - T_1)$$

- Derive an expression for the temperature distribution  $T(x)$  in symbolic form, assuming one-dimensional conditions. Sketch the temperature distribution.
- Calculate the heat rate  $q_x$ .

$$\frac{4q_x}{\pi a^2} \ln\left(\frac{x}{x_1}\right) = -k(T - T_1)$$

$$q_x = \frac{-k(T - T_1) \pi a^2}{4 \ln\left(\frac{x}{x_1}\right)}$$

$$= \frac{-k(400\text{ K} - 600\text{ K}) \pi (0.5\text{ m}^{1/2})^2}{4 \ln\left(\frac{125\text{ mm}}{25\text{ mm}}\right)} =$$