

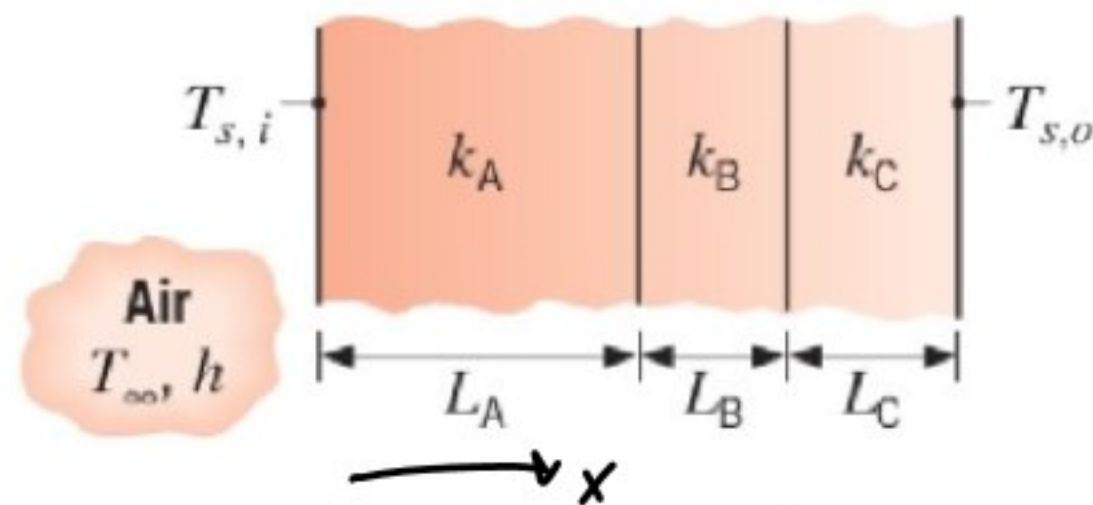
$$q'' = h(T_{s,i} - T_{\infty})$$

$$q'' = 25 \frac{\text{W}}{\text{m}^2 \cdot \text{K}} (600^\circ\text{C} - 800^\circ\text{C})$$

$$q'' = 25 \frac{\text{W}}{\text{m}^2 \cdot \text{K}} (-200 \text{K})$$

$$= -5000 \frac{\text{W}}{\text{m}^2}$$

The composite wall of an oven consists of three materials, two of which are of known thermal conductivity,  $k_A = 25 \text{ W/m} \cdot \text{K}$  and  $k_C = 60 \text{ W/m} \cdot \text{K}$ , and known thickness,  $L_A = 0.40 \text{ m}$  and  $L_C = 0.20 \text{ m}$ . The third material, B, which is sandwiched between materials A and C, is of known thickness,  $L_B = 0.20 \text{ m}$ , but unknown thermal conductivity  $k_B$ .



Under steady-state operating conditions, measurements reveal an outer surface temperature of  $T_{s,o} = 20^\circ\text{C}$ , an inner surface temperature of  $T_{s,i} = 600^\circ\text{C}$ , and an oven air temperature of  $T_{\infty} = 800^\circ\text{C}$ . The inside convection coefficient  $h$  is known to be  $25 \text{ W/m}^2 \cdot \text{K}$ . What is the value of  $k_B$ ?

$$R_A = \frac{L_A}{k_A A}$$

$$= \frac{0.4 \text{ m}}{25 \frac{\text{W}}{\text{m} \cdot \text{K}} A}$$

$$= \frac{0.016 \frac{\text{m}^2 \cdot \text{K}}{\text{W}}}{A}$$



$$R_B = \frac{L_B}{k_B A} = \frac{0.2 \text{ m}}{k_B A}$$

$$R_C = \frac{L_C}{k_C A} = \frac{0.2 \text{ m}}{60 \frac{\text{W}}{\text{mK}} A} = \frac{0.033}{A} \frac{\text{m}^2 \text{K}}{\text{W}}$$

$$R_e = R_A + R_B + R_C = \frac{0.016}{A} \frac{\text{m}^2 \text{K}}{\text{W}} + \frac{0.2 \text{ m}}{k_B A} + \frac{0.033}{A} \frac{\text{m}^2 \text{K}}{\text{W}} = \frac{0.049}{A} \frac{\text{m}^2 \text{K}}{\text{W}} + \frac{0.2 \text{ m}}{k_B A}$$

$$\frac{T_{so} - T_{si}}{q} = \frac{0.049}{A} \frac{\text{m}^2 \text{K}}{\text{W}} + \frac{0.2 \text{ m}}{k_B A}$$

$$\frac{T_{so} - T_{si}}{q''} = 0.049 \frac{\text{m}^2 \text{K}}{\text{W}} + \frac{0.2 \text{ m}}{k_B}$$

$$\frac{20^{\circ}\text{C} - 100^{\circ}\text{C}}{-5000 \frac{\text{W}}{\text{m}^2}} = 0.049 \frac{\text{m}^2\text{K}}{\text{W}} + \frac{0.2 \text{ m}}{K_B}$$

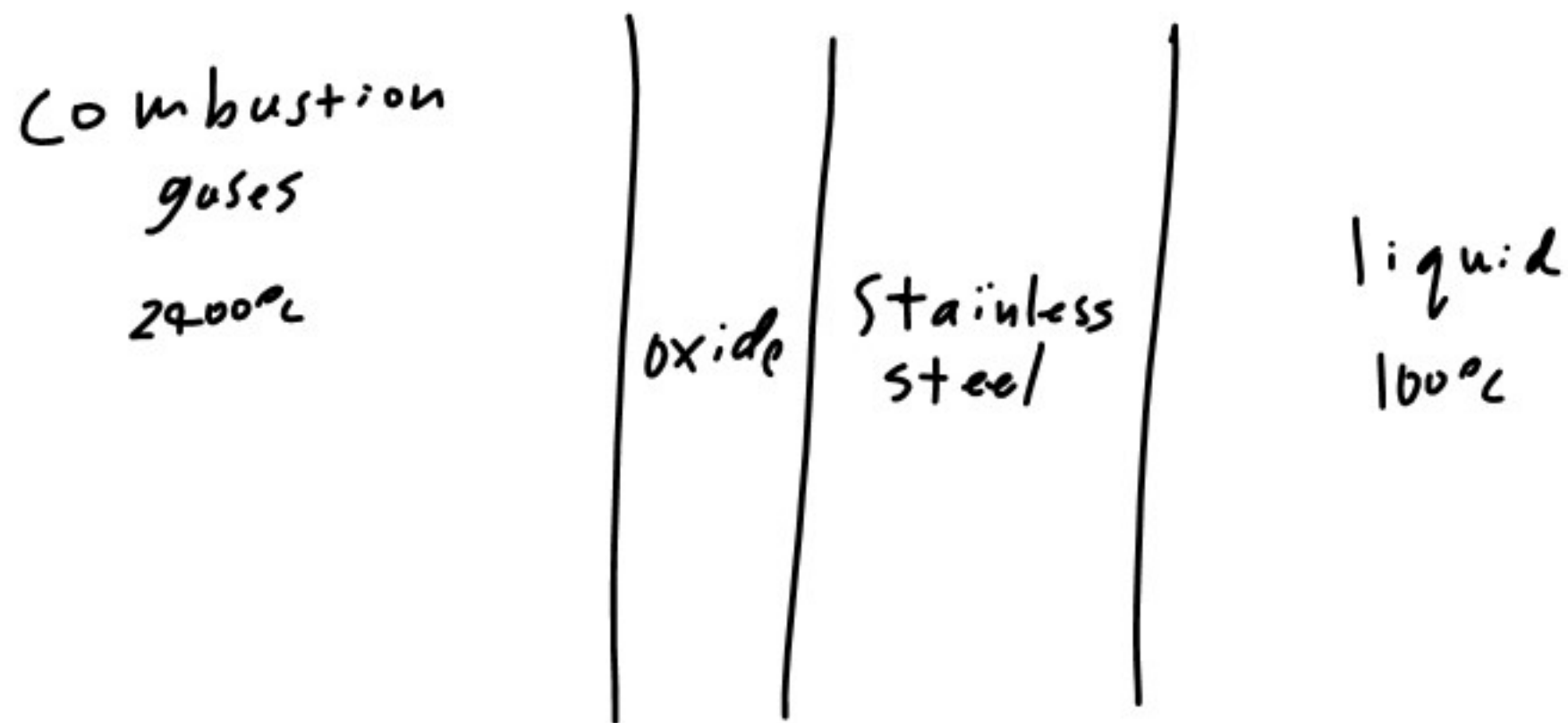
$$\frac{-580 \text{ K}}{-5000 \frac{\text{W}}{\text{m}^2}} = 0.049 \frac{\text{m}^2\text{K}}{\text{W}} + \frac{0.2 \text{ m}}{K_B}$$

$$0.116 \frac{\text{K m}^2}{\text{W}} - 0.049 \frac{\text{m}^2\text{K}}{\text{W}} = \frac{0.2 \text{ m}}{K_B}$$

$$0.067 \frac{\text{K m}^2}{\text{W}} = \frac{0.2 \text{ m}}{K_B}$$

$$K_B = \frac{0.2 \text{ m}}{0.067 \frac{\text{K m}^2}{\text{W}}} = \boxed{3 \frac{\text{W}}{\text{mK}}}$$

A composite wall separates combustion gases at  $2400^{\circ}\text{C}$  from a liquid coolant at  $100^{\circ}\text{C}$ , with gas and liquid-side convection coefficients of  $25$  and  $1000 \text{ W/m}^2 \cdot \text{K}$ . The wall is composed of a  $12\text{-mm}$ -thick layer of beryllium oxide on the gas side and a  $24\text{-mm}$ -thick slab of stainless steel (AISI 304) on the liquid side. The contact resistance between the oxide and the steel is  $0.05 \text{ m}^2 \cdot \text{K/W}$ . What is the rate of heat loss per unit surface area of the composite? Sketch the temperature distribution from the gas to the liquid.



$$R_e = R_{conv,g} + R_{cond,o} + R_{cont} + R_{cond,s} + R_{conv,l}$$

$$R_{conv,g} = \frac{1}{hA} = \frac{1}{25 \frac{W}{m^2K} A}$$

$$R_{conv,l} = \frac{1}{hA} = \frac{1}{1000 \frac{W}{m^2K} A}$$

$$R_{cont} = \frac{0.05 \frac{m^2K}{W}}{A}$$

$$R_{cond,o} = \frac{L}{KA} = \frac{0.012 m}{272 \frac{W}{mK} A}$$

$$R_{cond,s} = \frac{L}{KA} = \frac{0.024}{19.9 \frac{W}{mK} A}$$

$$R_c = \frac{1}{25 \frac{\text{W}}{\text{m}^2\text{K}}} A + \frac{1}{1000 \frac{\text{W}}{\text{m}^2\text{K}}} A + \frac{0.05 \frac{\text{m}^2\text{K}}{\text{W}}}{A} + \frac{0.012 \text{ m}}{272 \frac{\text{W}}{\text{mK}}} A + \frac{0.029 \text{ m}}{19.9 \frac{\text{W}}{\text{mK}}} A$$