



**3.102** A long, circular aluminum rod is attached at one end to a heated wall and transfers heat by convection to a cold fluid.

- (a) If the diameter of the rod is doubled, by how much would the rate of heat removal change?
- (b) If a copper rod of the same diameter is used in place of the aluminum, by how much would the rate of heat removal change?

$$k_a = 237 \frac{\text{W}}{\text{mK}}$$

$$k_c = 401 \frac{\text{W}}{\text{mK}}$$

$$M = \sqrt{h P k A_c} \quad \theta_b = q_{\text{f}}$$

$$\sqrt{h P k \frac{\pi d^2}{4}} \theta_b = \frac{d}{2} \sqrt{h P k \pi} \theta_b$$

$$A_c = \frac{\pi d^2}{4}$$

$$q_{\text{f}c} = a q_{\text{f}a}$$

$$\sqrt{h P k_c A_c} \theta_b = a \sqrt{h P k_a A_c} \theta_b$$

$$\sqrt{k_c} = a \sqrt{k_a}$$

$$a = \sqrt{\frac{k_c}{k_a}}$$

**5.10** A steel sphere (AISI 1010), 100 mm in diameter, is coated with a dielectric material layer of thickness 2 mm and thermal conductivity 0.04 W/m · K. The coated sphere is initially at a uniform temperature of 500°C and is suddenly quenched in a large oil bath for which  $T_\infty = 100^\circ\text{C}$  and  $h = 3000 \text{ W/m}^2 \cdot \text{K}$ . Estimate the time required for the coated sphere temperature to reach 150°C. *Hint:* Neglect the effect of energy storage in the dielectric material, since its thermal capacitance ( $\rho c V$ ) is small compared to that of the steel sphere.

$$k = 63.9 \frac{\text{W}}{\text{m} \cdot \text{K}}$$

$$\rho = 7832 \frac{\text{kg}}{\text{m}^3}$$

$$c = 439 \frac{\text{J}}{\text{kg} \cdot \text{K}}$$

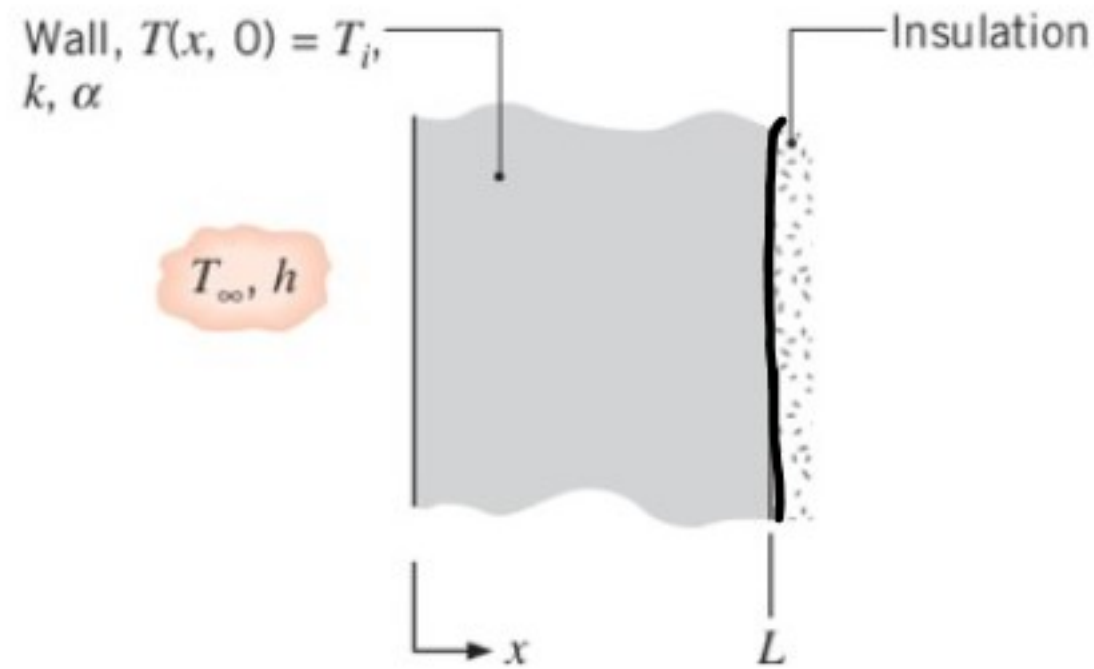
$$Bi = \frac{hL_c}{k} = \frac{3000 \frac{\text{W}}{\text{m}^2 \cdot \text{K}} \cdot 0.05 \text{ m}}{63.9 \frac{\text{W}}{\text{m} \cdot \text{K}}}$$

$$\theta = T - T_\infty = 150^\circ\text{C} - 100^\circ\text{C} = 50 \text{ K}$$

$$\theta_i = 500^\circ\text{C} - 100^\circ\text{C} = 400 \text{ K}$$

$$\frac{\theta}{\theta_i} = \exp\left(-\frac{hA_s}{\rho V c} t\right) = 0.0068$$

**5.36** Consider the one-dimensional wall shown in the sketch, which is initially at a uniform temperature  $T_i$  and is suddenly subjected to the convection boundary condition with a fluid at  $T_\infty$ .



$$\theta^* = C_1 \exp(-\beta_1^2 Fo) \cos(\beta_1 x^*)$$

For a particular wall, case 1, the temperature at  $x = L_1$  after  $t_1 = 100$  s is  $T_1(L_1, t_1) = 315^\circ\text{C}$ . Another wall, case 2, has different thickness and thermal conditions as shown.

Case	$L$ (m)	$\alpha$ ( $\text{m}^2/\text{s}$ )	$k$ ( $\text{W}/\text{m} \cdot \text{K}$ )	$T_i$ ( $^\circ\text{C}$ )	$T_\infty$ ( $^\circ\text{C}$ )	$h$ ( $\text{W}/\text{m}^2 \cdot \text{K}$ )
1	0.10	$15 \times 10^{-6}$	50	300	400	200
2	0.40	$25 \times 10^{-6}$	100	30	20	100

How long will it take for the second wall to reach  $28.5^\circ\text{C}$  at the position  $x = L_2$ . Use as the basis for analysis, the dimensionless functional dependence for the transient temperature distribution expressed in Equation 5.41.

$$\theta^* = \frac{T - T_\infty}{T_i - T_\infty} \quad Fo = \frac{\alpha t}{L^2} \quad x^* = \frac{x}{L} = 1$$