



**7.36** A long, cylindrical, electrical heating element of diameter  $D = 12$  mm, thermal conductivity  $k = 240$  W/m · K, density  $\rho = 2700$  kg/m<sup>3</sup>, and specific heat  $c_p = 900$  J/kg · K is installed in a duct for which air moves in cross flow over the heater at a temperature and velocity of  $30^\circ\text{C}$  and  $8$  m/s, respectively.

- (a) Neglecting radiation, estimate the steady-state surface temperature when, per unit length of the heater, electrical energy is being dissipated at a rate of  $1000$  W/m.
- (b) If the heater is activated from an initial temperature of  $30^\circ\text{C}$ , estimate the time required for the surface temperature to come within  $10^\circ\text{C}$  of its steady-state value.

$$Re_D = \frac{V D}{\nu} = \frac{8 \text{ m/s} \cdot 0.012 \text{ m}}{32.39 \times 10^{-6} \text{ m}^2/\text{s}} = 2969$$
$$T_f = 450 \text{ K}$$
$$\nu = 32.39 \times 10^{-6} \frac{\text{m}^2}{\text{s}}$$

$$\overline{Nu_D} = C Re_D^m Pr^{1/3} = 0.683 (2969)^{0.466} 0.606^{1/3} = 25$$

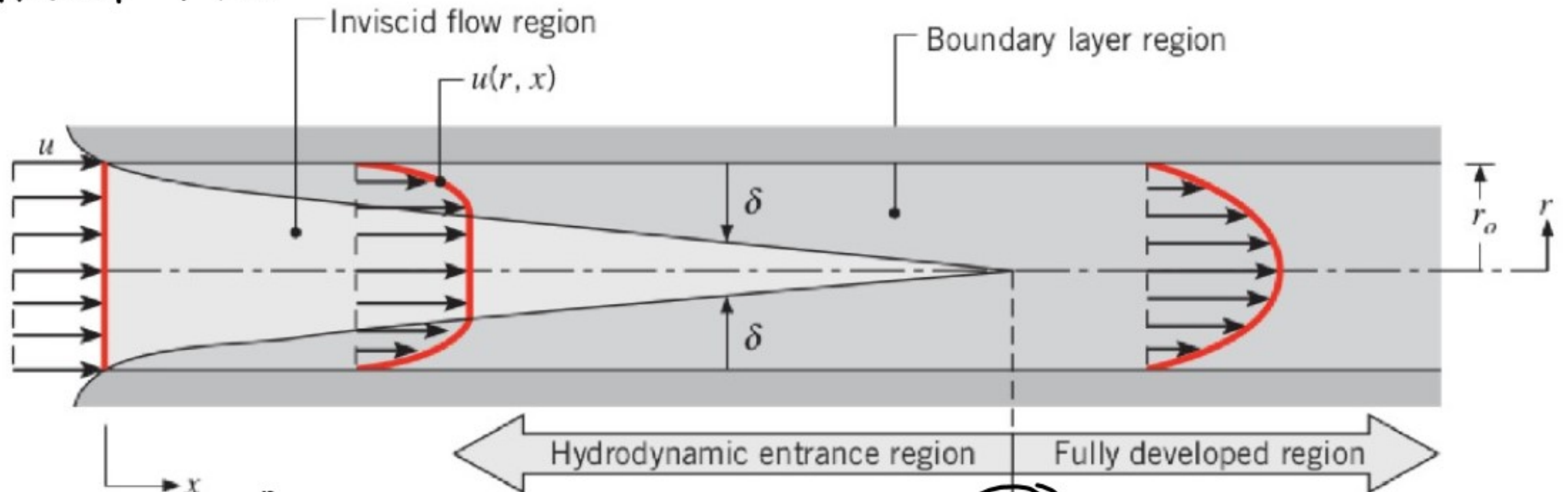
$$\overline{Nu_D} = 0.3 + \frac{0.62 Re_D^{1/2} Pr^{1/3}}{\left(1 + \left(\frac{0.7}{Pr}\right)^{1/4}\right)^{1/4}} \left(1 + \left(\frac{Re_D}{232000}\right)^{5/3}\right)^{4/5} = 27.6$$

$$\overline{Nu_D} = \frac{\bar{h} D}{k} \quad \bar{h} = \frac{k}{D} \overline{Nu_D} = \frac{0.0373 \frac{W}{mK}}{0.012 m} 27.6 = 85.7 \frac{W}{m^2 K}$$

$$\frac{T - T_\infty}{T_i - T_\infty} = \frac{b/a}{T_i - T_\infty} = \frac{b}{a} = \frac{\dot{E}_g}{\frac{h A_s}{\cancel{pvc}}} = \frac{\dot{E}_g}{h A_s} = \frac{1000 \frac{W}{m}}{85.7 \frac{W}{m^2 K} \pi 0.012 m}$$

$$T = 612 K$$

# Internal Flow



$$Re_D = \frac{\rho U_m D}{\mu} = \frac{U_m D}{\nu}$$

$U_m$  mean fluid velocity

$x_{fd,h}$

$Re_{Dc} = 2300$  critical Reynolds Number

Laminar

$$\left( \frac{x_{fd,h}}{D} \right)_{lam} = 0.05 Re_D$$