

8.20 Engine oil flows through a 25-mm-diameter tube at a rate of 0.5 kg/s. The oil enters the tube at a temperature of 25°C, while the tube surface temperature is maintained at 100°C.

$$Re_D = \frac{\dot{m}}{\pi D \mu} = \frac{0.5 \text{ kg/s}}{\pi \cdot 0.025 \text{ m} \cdot 78.6 \times 10^{-2} \frac{\text{Ns}}{\text{m}^2}} = 52.4$$

(a) Determine the oil outlet temperature for a 5-m and for a 100-m long tube. For each case, compare the log mean temperature difference to the arithmetic mean temperature difference.

$$Pr = 6400$$

$$k = 195 \times 10^{-3} \frac{\text{W}}{\text{m K}}$$

$$\bar{h} = \frac{k}{D} \overline{Nu_D} = \frac{k}{D} \left(3.66 + \frac{0.0688 \frac{D}{L} Re_D Pr}{1 + 0.04 \left(\frac{D}{L} Re_D Pr \right)^{2/3}} \right) = \frac{195 \times 10^{-3}}{0.025} \left(3.66 + \frac{0.0688 \frac{0.025}{5} 52.4 \cdot 6400}{1 + 0.04 \left(\frac{0.025}{5} 52.4 \cdot 6400 \right)^{2/3}} \right)$$

$$= 122 \frac{\text{W}}{\text{m}^2 \text{K}}$$

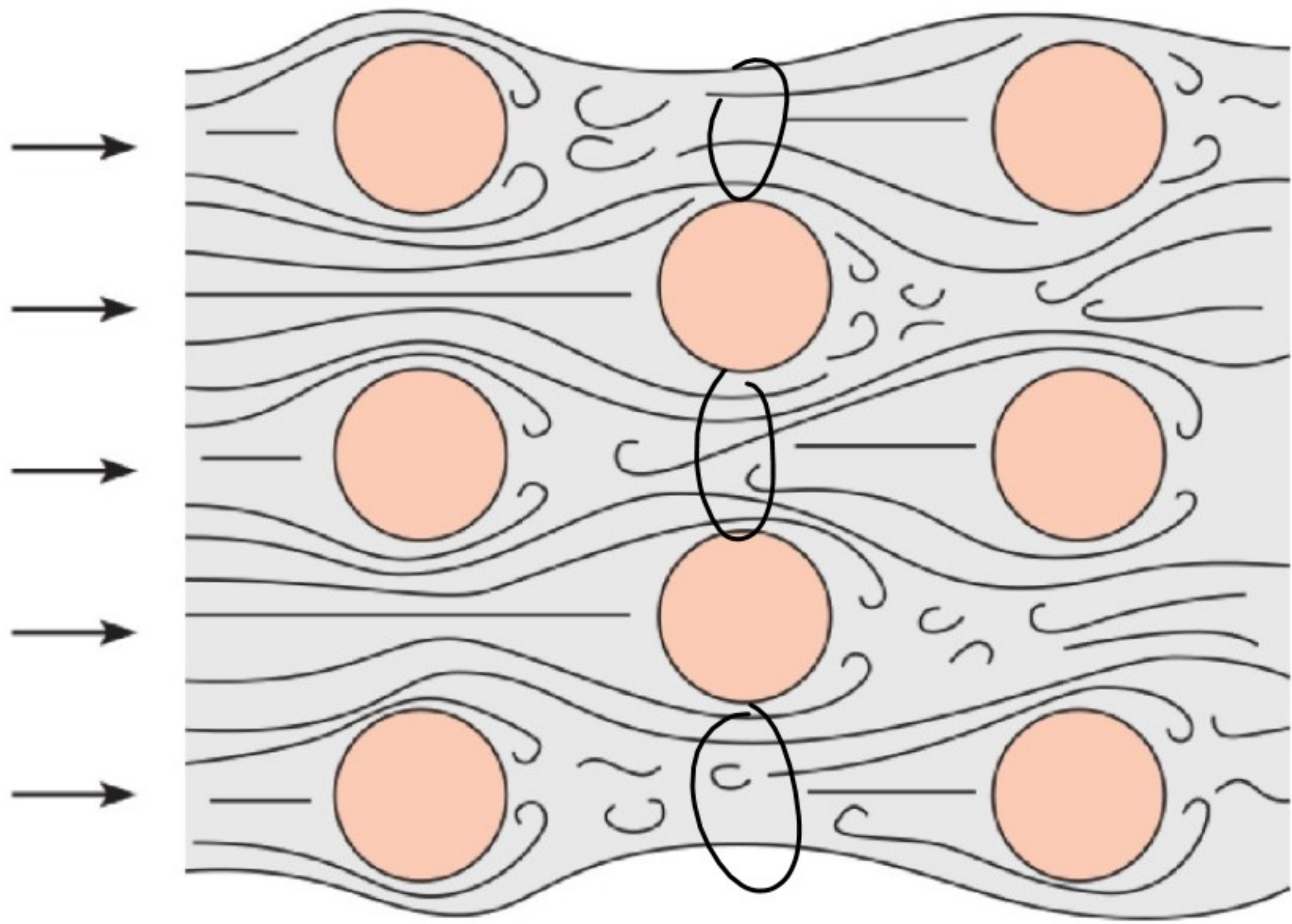
$$\frac{T_s - T_{m0}}{T_s - T_{mi}} = \exp\left(-\frac{PL}{\dot{m} c_p} \bar{h}\right)$$

$$\frac{100^\circ\text{C} - T_{m0}}{100^\circ\text{C} - 25^\circ\text{C}} = \exp\left(-\frac{\pi \cdot 0.025 \cdot 5}{0.5 \cdot 1909} \cdot 122\right) = 0.95$$

$$100^\circ\text{C} - T_{m0} = 0.95 (100^\circ\text{C} - 25^\circ\text{C})$$

$$-T_{m0} = 0.95 (75^\circ\text{C}) - 100^\circ\text{C} = -28.7^\circ\text{C}$$

$$\boxed{T_{m0} = 28.7^\circ\text{C}}$$



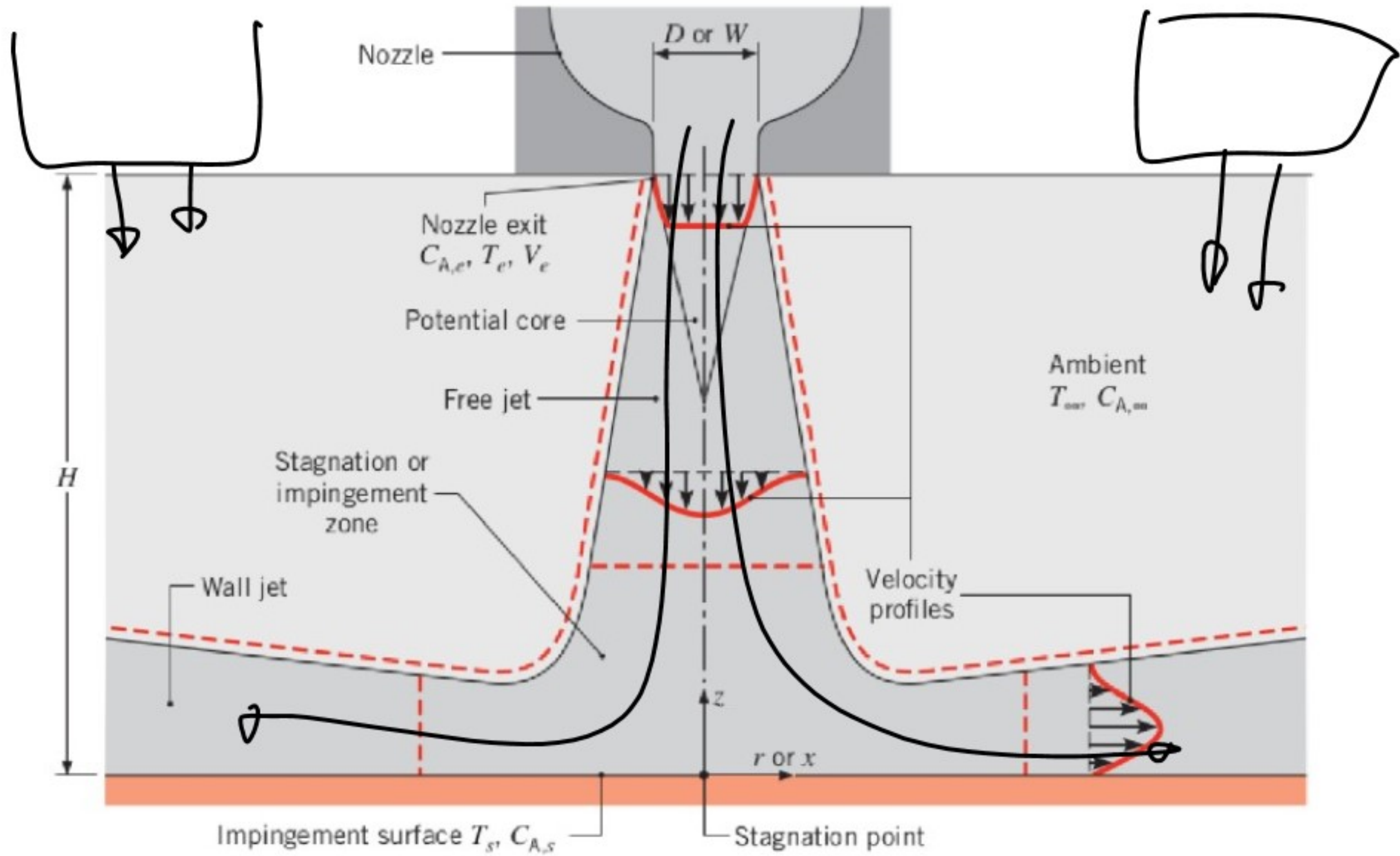


TABLE 8.1 Nusselt numbers and friction factors for fully developed laminar flow in tubes of differing cross section


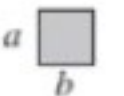


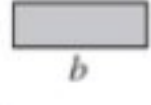

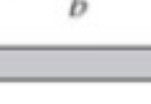



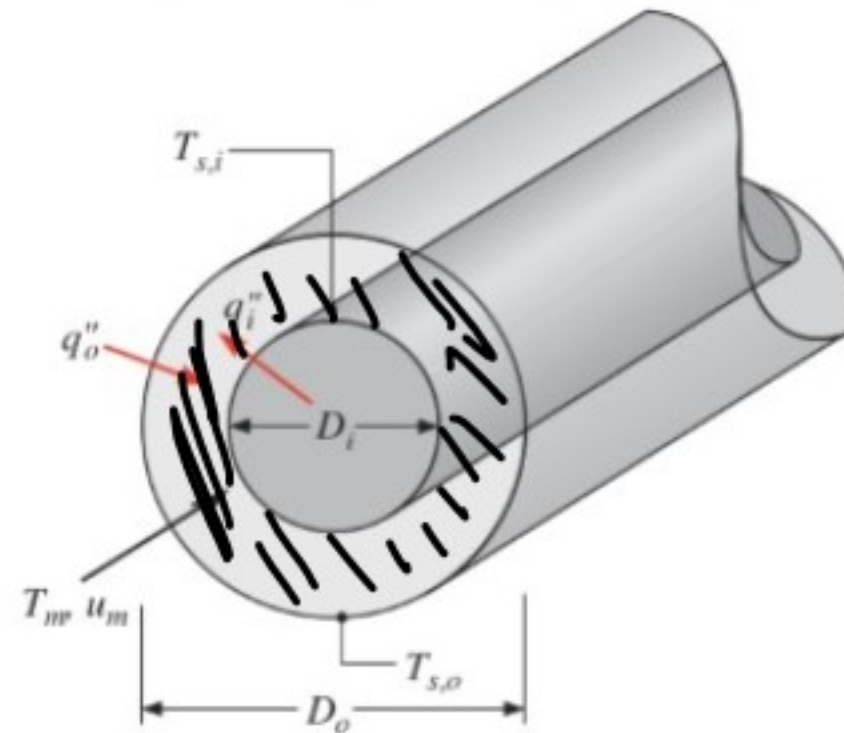
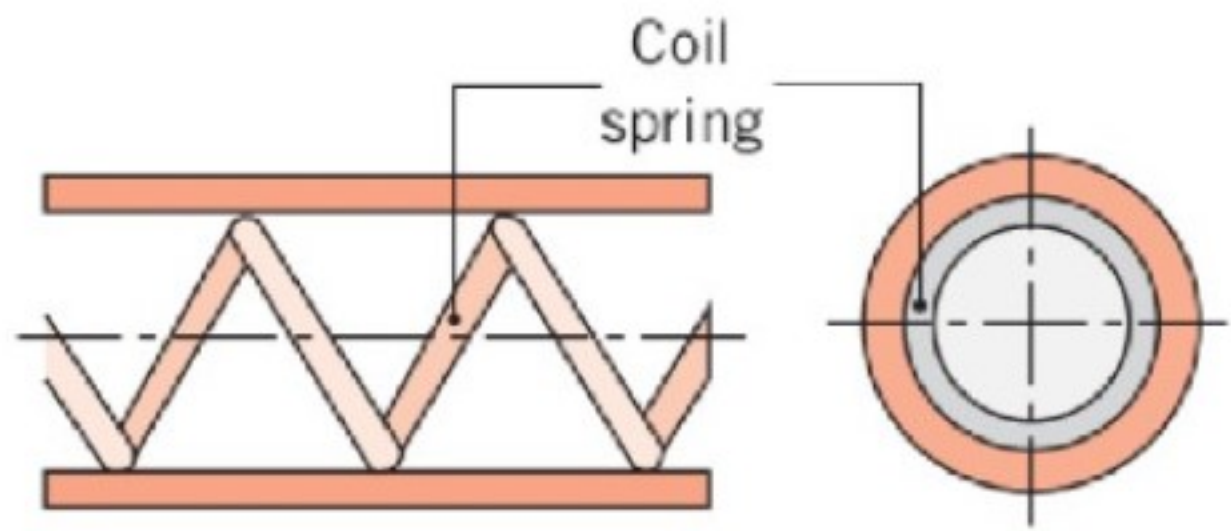
Cross Section	$\frac{b}{a}$	$Nu_D \equiv \frac{hD_h}{k}$		fRe_{D_h}
		(Uniform q_s'')	(Uniform T_s)	
	—	4.36	<u>3.66</u>	64
	1.0	3.61	<u>2.98</u>	57
	1.43	3.73	3.08	59
	2.0	4.12	3.39	62
	3.0	4.79	3.96	69
	4.0	5.33	4.44	73
	8.0	6.49	5.60	82
	<u>∞</u>	8.23	<u>7.54</u>	96
	∞	5.39	<u>4.86</u>	96
	—	3.11	<u>2.49</u>	53

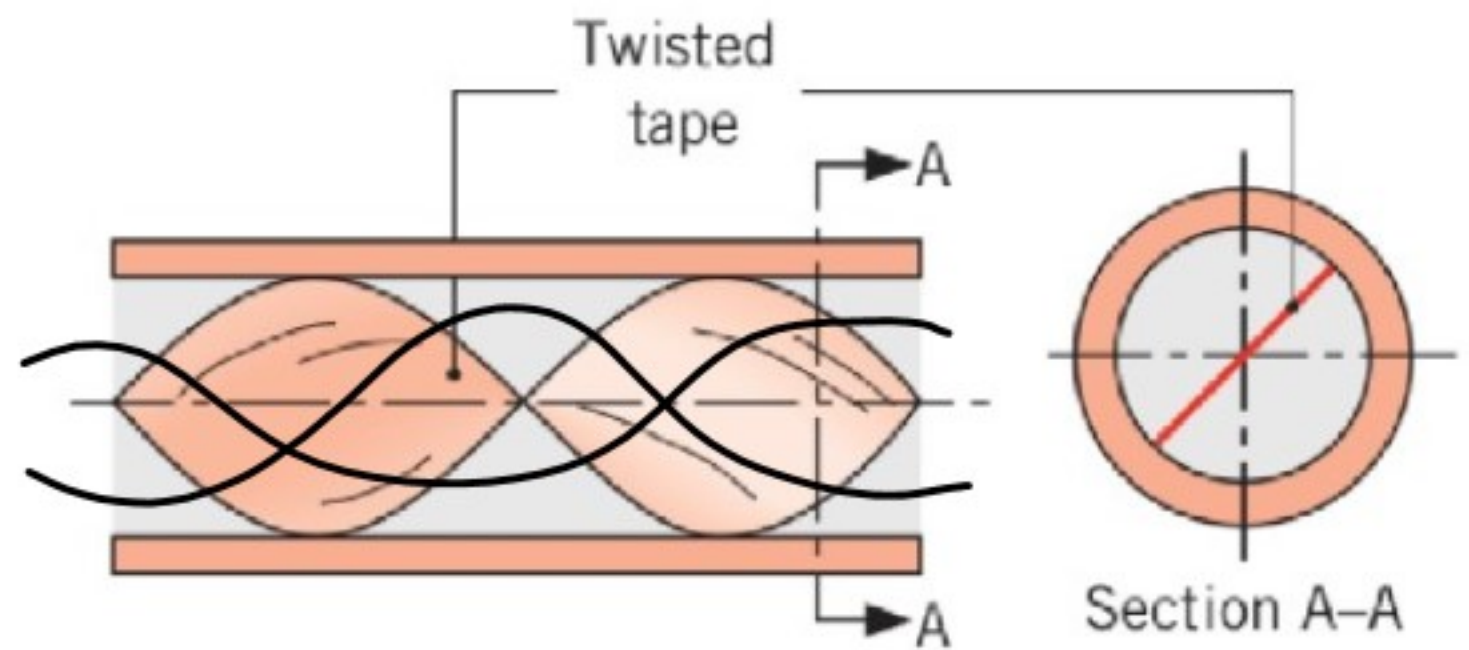
TABLE 8.2 Nusselt number for fully developed laminar flow in a circular tube annulus with one surface insulated and the other at constant temperature

D_i/D_o	Nu_i	Nu_o	Comments
0	—	3.66	See Equation 8.55
0.05	17.46	4.06	
0.10	11.56	4.11	
0.25	7.37	4.23	
0.50	5.74	4.43	
≈ 1.00	4.86	4.86	See Table 8.1, $b/a \rightarrow \infty$

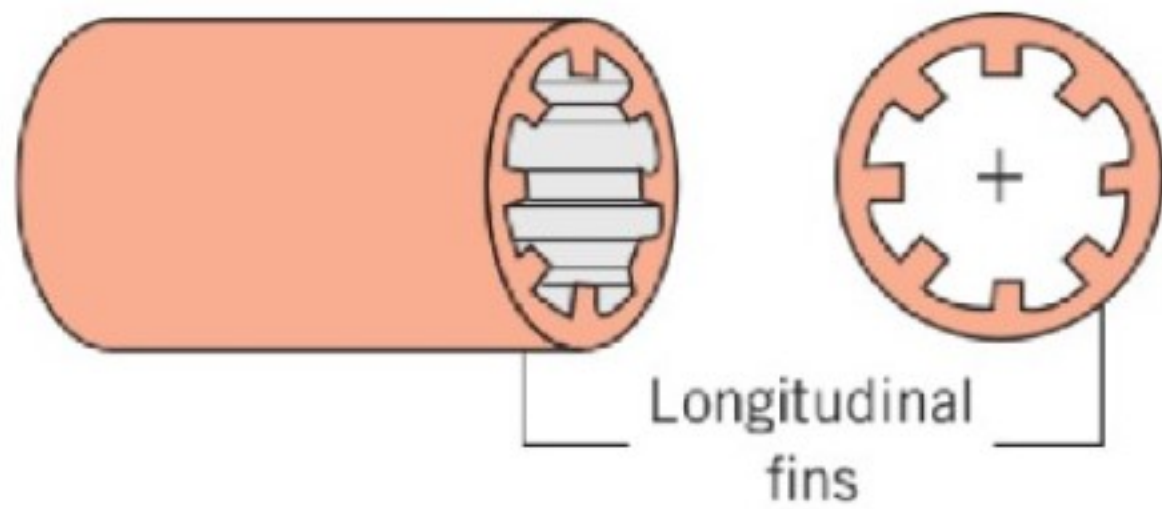




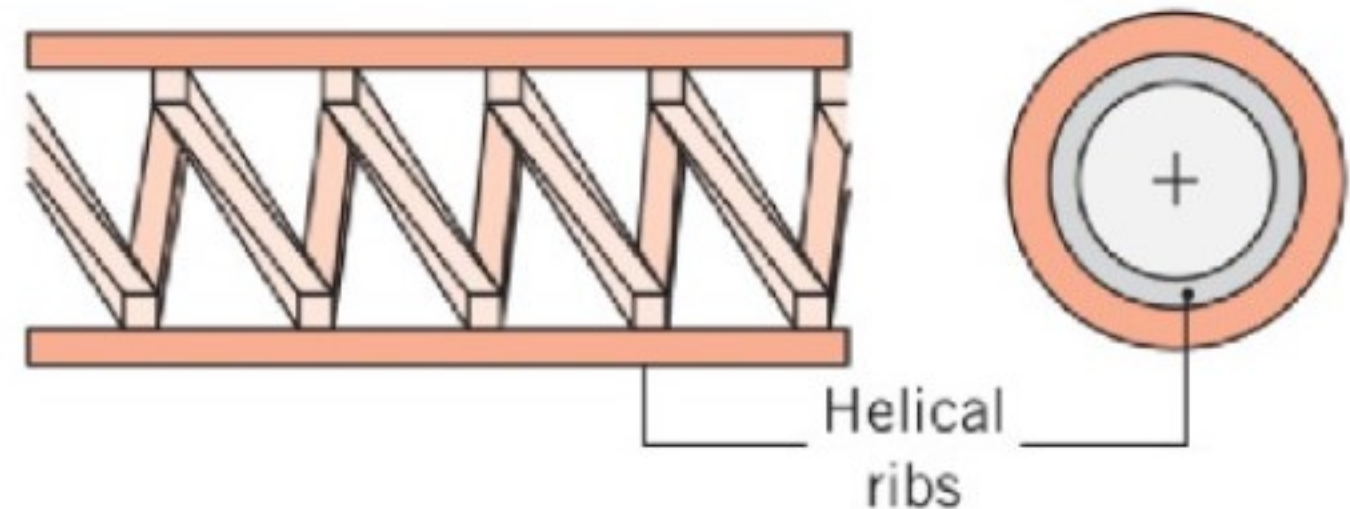
(a)



(b)

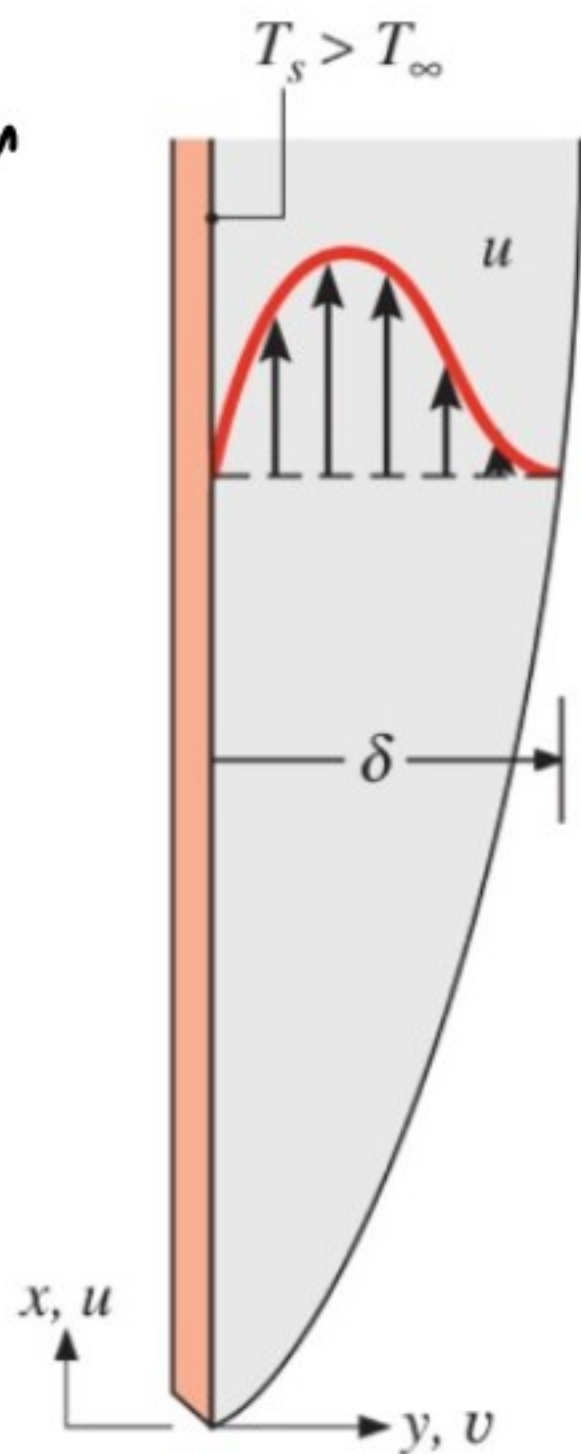


(c)



(d)

Free Convection

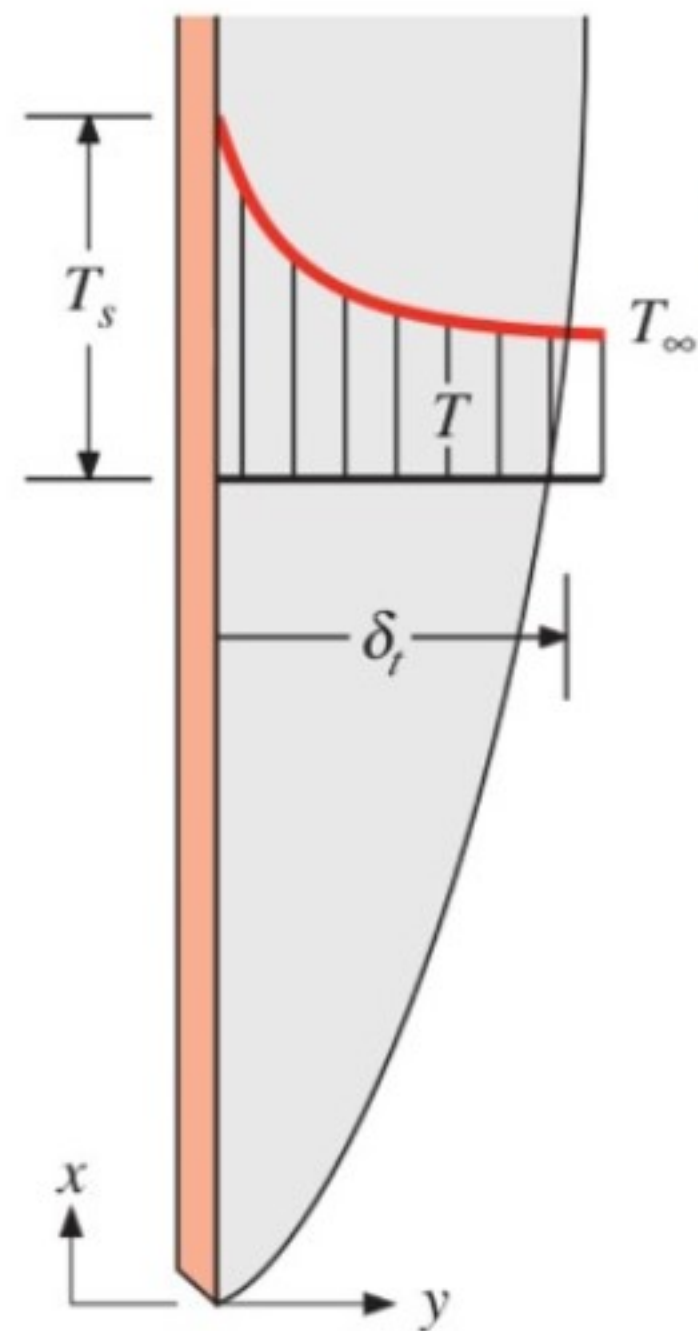


(a)

Quiescent fluid

T_∞, ρ_∞

g



(b)

Quiescent fluid

T_∞, ρ_∞

g